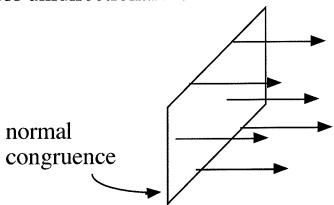
METR 5113, Advanced Atmospheric Dynamics I Alan Shapiro, Instructor Wednesday, 5 September 2018 (lecture 7)

- Day/time for exams and make-ups: Fridays 9-11 am
- 2 handouts: normal congruence, answers to prob set 1.

Normal congruence

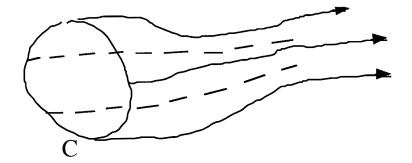
A sfc that is everywhere \perp to the flow is a "normal congruence" e.g. for unidirectional flow:



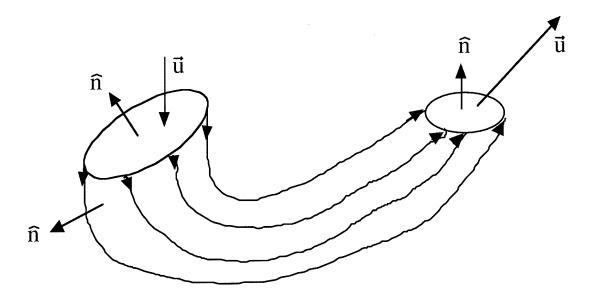
Can such a sfc be constructed in all flows? No! Only in flows that have no helicity, i.e., only if $\vec{u} \cdot (\nabla \times \vec{u}) = 0$. $(\vec{u} \cdot \vec{\omega} = 0$, where $\vec{\omega} \equiv \nabla \times \vec{u}$ is vorticity). See optional handout for details.

Streamtubes

Consider arbitrary <u>closed</u> curve C drawn in the flow at a given time. Through each point of C draw a streamline. The sfc swept out by these streamlines is a <u>streamtube</u>. It's a sfc that's everywhere tangent to local velocity vectors. A streamtube behaves kinematically like a pipe (no flow \perp to sidewalls).



Consider volume V enclosed by chunk of a streamtube:



 $\hat{\mathbf{n}}$ is local unit outward normal to the <u>closed sfc</u> A bounding V (A is streamtube + 2 end-faces). $\hat{\mathbf{n}}$ on streamtube is \perp to flow.

If flow is <u>incompressible</u> (3D non-divergent, $\nabla \cdot \vec{u} = 0$) the lhs of div thm $\int_{V} \nabla \cdot \vec{u} \, dV = \int_{A} \vec{u} \cdot \hat{n} \, dA$ is 0, so rhs is 0: $\int_{A} \vec{u} \cdot \hat{n} \, dA = 0$

$$\therefore \int_{\text{face1}} \vec{\mathbf{u}} \cdot \hat{\mathbf{n}} \, d\mathbf{A} + \int_{\text{face2}} \vec{\mathbf{u}} \cdot \hat{\mathbf{n}} \, d\mathbf{A} + \int_{\text{streamtube}} \vec{\mathbf{u}} \cdot \hat{\mathbf{n}} \, d\mathbf{A} = 0$$

$$0 \text{ since } \vec{\mathbf{u}} \cdot \hat{\mathbf{n}} = 0 \text{ on streamtube}$$

$$\therefore \int_{\text{face1}} \vec{\mathbf{u}} \cdot \hat{\mathbf{n}} \, d\mathbf{A} = -\int_{\text{face2}} \vec{\mathbf{u}} \cdot \hat{\mathbf{n}} \, d\mathbf{A}$$

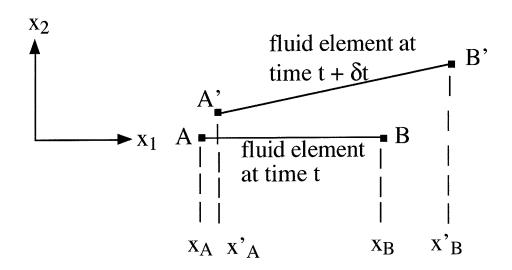
 $\therefore \quad \int \vec{u} \cdot \hat{n} \, dA \quad \text{is } \underline{\text{equal and opposite}} \text{ on the 2 end-faces}.$

Rate of mass transport <u>inward</u> across one face equals rate of mass transport <u>outward</u> across other face. If a face is small, the velocity is (relatively) large.

Strain rates in a fluid

"Normal" or "linear" rate of strain is <u>rate of change in length of a linear fluid element per unit length of the element</u>. (elements are infinitesimal).

Consider infinitesimal linear fluid element initially aligned in x_1 dirⁿ. Linear rate of strain of this element is $\lim_{\delta x_1 \to 0} \frac{1}{\delta x_1} \frac{D\delta x_1}{Dt}$. Relate it to flow field.



[Figure depicts translation, stretching and rotation. Fluid element is so small that velocity varies at most linearly across it, i.e., h.o.t. in Taylor expansion drop out.]

For small δt , elongation of this x_1 -oriented element is due only to stretching in x_1 direction. Rotation and translation don't elongate the element. So don't worry about them.

Length of element at time t:

$$\delta x_1(t) = x_B - x_A$$

Length of element at time $t + \delta t$:

$$\delta x_1(t + \delta t) = x'_B - x'_A$$

$$x'_B = x_B + u_B \delta t + h.o.t.$$

$$x'_A = x_A + u_A \delta t + h.o.t.$$

$$\therefore x'_{B} - x'_{A} = x_{B} - x_{A} + (u_{B} - u_{A}) \delta t + h.o.t.$$

$$\therefore \quad \delta x_1(t + \delta t) = \delta x_1(t) + (u_B - u_A) \delta t + h.o.t.$$

$$\begin{split} \delta x_1(t+\delta t) &- \delta x_1(t) = \left(\underline{u_B} - u_A \right) \delta t + \text{h.o.t.} \\ &\downarrow \quad \text{Taylor expansion for } u_B \text{:} \\ u_B &= u_A + \frac{\partial u_1}{\partial x_1} \delta x_1 + \text{h.o.t.} \end{split}$$

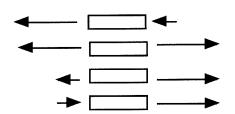
$$\therefore \quad \delta x_1(t + \delta t) - \delta x_1(t) = \frac{\partial u_1}{\partial x_1} \delta x_1 \delta t + \text{h.o.t.}$$

÷ by $\delta x_1 \delta t$ and let $\delta x_1 \rightarrow 0$, $\delta t \rightarrow 0$ to get linear rate of strain:

$$\lim_{\begin{subarray}{c} \delta x_1 \to 0 \\ \delta t \to 0 \end{subarray}} \frac{\delta x_1(t + \delta t) - \delta x_1(t)}{\delta x_1 \, \delta t} = \frac{\partial u_1}{\partial x_1}$$

or,
$$\frac{1}{\delta x_1} \frac{D\delta x_1}{Dt} = \frac{\partial u_1}{\partial x_1}$$
 (in limit of vanishing δx_1)

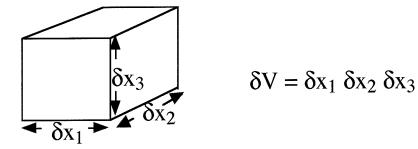
e.g., flows with $\partial u_1/\partial x_1 > 0$:



Similar analysis of x_2 - and x_3 -oriented blobs leads to:

$$\frac{1}{\delta x_2} \frac{D\delta x_2}{Dt} = \frac{\partial u_2}{\partial x_2}, \quad \text{and} \quad \frac{1}{\delta x_3} \frac{D\delta x_3}{Dt} = \frac{\partial u_3}{\partial x_3}.$$

Volumetric rate of strain: relative rate of change in volume of an infinitesimal fluid box: $\frac{1}{\delta V} \frac{D\delta V}{Dt}$



Relate vol rate of strain to the flow field:

$$\begin{split} &\frac{1}{\delta V}\frac{D\delta V}{Dt} = \frac{1}{\delta x_1 \delta x_2 \delta x_3} \frac{D}{Dt} \left(\delta x_1 \delta x_2 \delta x_3 \right) \\ &= \frac{1}{\delta x_1 \delta x_2 \delta x_3} \left[\delta x_2 \delta x_3 \frac{D\delta x_1}{Dt} + \delta x_1 \delta x_3 \frac{D\delta x_2}{Dt} + \delta x_1 \delta x_2 \frac{D\delta x_3}{Dt} \right] \\ &= \frac{1}{\delta x_1} \frac{D\delta x_1}{Dt} + \frac{1}{\delta x_2} \frac{D\delta x_2}{Dt} + \frac{1}{\delta x_3} \frac{D\delta x_3}{Dt} \\ &= \frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3} = \frac{\partial u_i}{\partial x_i} = \nabla \cdot \vec{u} \end{split}$$
 So
$$\frac{1}{\delta V} \frac{D\delta V}{Dt} = \nabla \cdot \vec{u} \qquad \text{(in limit of vanishing box size)}$$

So if flow is non-divergent $(\nabla \cdot \vec{\mathbf{u}} = 0)$, fluid elements do not change their volume (though they can change their shape).