

Prototypical natural convection flows:
Plumes and Thermals

Some good references:

Batchelor 1954 QJRM S

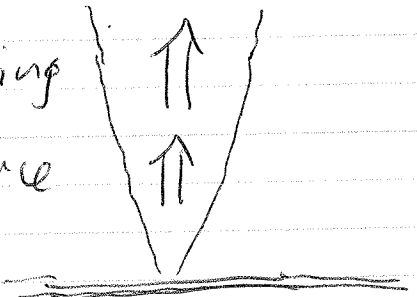
Morton, Taylor, and Turner 1956 Proc. Roy. Soc. London, A

Emanuel's textbook on convection

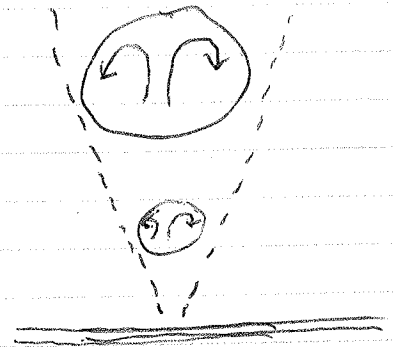
Turner's book on Buoyancy Effects in Fluids

Fannelöp's book: Fluid Mechanics for Industrial Safety and Environmental Protection, 2012

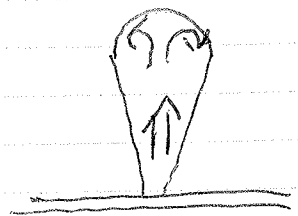
Plumes: Spatially continuous buoyant regions arising from a maintained point, line, or areal source of buoyancy.



Thermals: Discrete buoyant elements that arise from an impulsive or otherwise unsteady source of buoyancy.



Starting Plume: A plume in its development stage.

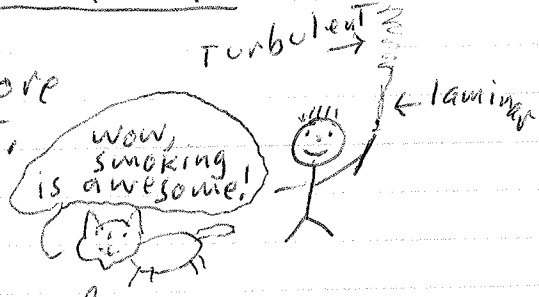


The simplest types of these flows arise from point or line singularities. Can be studied in the lab, in numerical experiments and in theoretical analyses (similarity models combined with the π theorem).

The main interest in these idealized flows is as "building blocks" in cumulus entrainment and as prototypical flow structures in the dry convective atmospheric boundary layer.

Batchelor's Theory for a laminar plume over a maintained point source of heat in an unstratified environment.

e.g. cigarette plume before it becomes turbulent.



- Consider statistical steady state
- Consider variations in temp T to be much smaller than T itself (so we'll invoke the Boussinesq approx).
- Consider atmosphere to be unstratified

Governing eq^{ns}:

Mass conservation
(well, incompressibility condⁿ) : $\nabla \cdot \vec{u} = 0$

Eqⁿ of motion
 $(\vec{u} \cdot \nabla) \vec{u} = -\frac{1}{\rho_0} \nabla P + \left(\frac{T - T_0}{T_0} \right) g \hat{k} + \nu \nabla^2 \vec{u}$
Annotations: ρ_0 (const density), T_0 (const temp), P (perturbation pressure)

Heat eqⁿ
(thermal energy eqⁿ) : $\vec{u} \cdot \nabla T = \kappa \nabla^2 T$

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Can rewrite heat eqⁿ in terms of the same buoyancy-like variable that appears in eqⁿ of motion:

$$\vec{v} \cdot \nabla \left[\left(\frac{T - T_0}{T_0} \right) g \right] = \kappa \nabla^2 \left[\left(\frac{T - T_0}{T_0} \right) g \right]$$

Look for approximate solutions in the form of similarity solutions (self-similarity solutions), i.e. solutions that look the same on every horizontal cross-section:


Other parameters of the problem (e.g. \vec{v} and κ) are also in here \rightarrow

$$\begin{cases}
 w = z^m \times \text{function}(r/R) \\
 g \left(\frac{T - T_0}{T_0} \right) = z^n \times \text{another function}(r/R) \\
 R = C z^l \text{ where } C \text{ is some constant}
 \end{cases}$$

Note: Proposing power laws in z goes beyond the similarity assumption, i.e. can look for height dependencies that are more general than power laws.

Note: We can interpret R as a measure of plume radius.

Consider axisymmetric flow due to a point source and assume that the diffusion term is dominated by changes in the radial direction, not the vertical dirⁿ, so:



$$\nabla^2(\) = \underbrace{\frac{\partial^2}{\partial z^2}(\)}_{\text{neglect}} + \frac{1}{r} \frac{\partial}{\partial r} r \frac{\partial}{\partial r}(\) + \frac{1}{r^2} \frac{\partial^2}{\partial \phi^2}(\)$$

Temp and \vec{v} change more rapidly in r direction than z direction

It's an internal boundary layer approximation, since flow is axisymmetric

(4)

$$\text{So } \nabla^2(\cdot) \approx \frac{1}{r} \frac{\partial}{\partial r} r \frac{\partial}{\partial r} (\cdot)$$

So now the steady state heat eqⁿ becomes:

$$\vec{v} \cdot \nabla \left[\left(\frac{T-T_0}{T_0} \right) g \right] = \frac{\kappa}{r} \frac{\partial}{\partial r} r \frac{\partial}{\partial r} \left[\left(\frac{T-T_0}{T_0} \right) g \right]$$

rewrite
l.h.s. as:

$$\nabla \cdot \left[\vec{v} \left(\frac{T-T_0}{T_0} \right) g \right]$$



scratch paper

for any scalar ϕ : $\nabla \cdot (\vec{v} \phi) = \phi \nabla \cdot \vec{v} + \vec{v} \cdot \nabla \phi$
 and since our flow is incompressible ($\nabla \cdot \vec{v} = 0$):
 $\nabla \cdot (\vec{v} \phi) = \vec{v} \cdot \nabla \phi$

Integrate this heat eqⁿ over a slab-like volume btw 2 z levels extending from $r=0$ to $r=\infty$:

$$\int_V \nabla \cdot \left[\vec{v} \left(\frac{T-T_0}{T_0} \right) g \right] dV = 2\pi \kappa \int \int \frac{1}{r} \frac{\partial}{\partial r} r \frac{\partial}{\partial r} \left[\left(\frac{T-T_0}{T_0} \right) g \right] r dr dz$$

these cancel!

where $dV = 2\pi r dr dz$
use this explicitly in the rhs integral

Use divergence th^m on l.h.s., get:

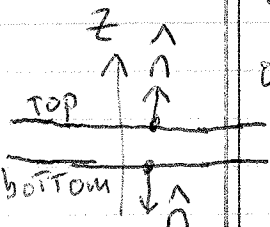
$$\int_A \vec{v} \left(\frac{T-T_0}{T_0} \right) g \cdot \hat{n} dA = 2\pi \kappa \int \int \frac{\partial}{\partial r} r \frac{\partial}{\partial r} \left[\left(\frac{T-T_0}{T_0} \right) g \right] dr dz$$

on lateral sides ($r \xrightarrow{\text{at}} \infty$): $T \rightarrow T_0$

and $\vec{v} \rightarrow 0$

so lateral integral drops out, only top/bottom area integrals survive.

can integrate w/ \vec{v} .



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$$\therefore \int_{\text{top area}} w \left(\frac{T-T_0}{T_0} \right) g dA - \int_{\text{bottom area}} w \left(\frac{T-T_0}{T_0} \right) g dA$$

$$= 2\pi K \int_{r=0}^{r=\infty} \left[r^2 \frac{\partial}{\partial r} \left(\frac{T-T_0}{T_0} \right) g \right] dz$$

The quantity [...] on the r.h.s. vanishes at $r=0$ (because of the r in it). If we assume that $T \rightarrow T_0$ sufficiently rapidly as $r \rightarrow \infty$ (e.g. if $T-T_0$ decays exponentially with r) then the r.h.s. $\rightarrow 0$.

$$\therefore \int_{\text{top area}} w \left(\frac{T-T_0}{T_0} \right) g dA = \int_{\text{bottom area}} w \left(\frac{T-T_0}{T_0} \right) g dA$$

but the top and bottom are at arbitrary heights so really we have:

$$\int_{\text{any infinite horizontal area}} w \left(\frac{T-T_0}{T_0} \right) g dA = \text{const, indep of } z$$

or, since $dA = 2\pi r dr$:

$$2\pi \int_0^{\infty} w g \left(\frac{T-T_0}{T_0} \right) r dr = \text{const, indep of } z$$

↑
call it F

Can interpret F as the heat flux, the rate at which heat is released by the source.

Rewrite this slightly so we can plug in our similarity expressions:

$$2\pi \int_0^{\infty} w g \left(\frac{T-T_0}{T_0} \right) R^2 \left(\frac{\Lambda}{R} \right) d\left(\frac{\Lambda}{R} \right) = F$$

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Now plug in the expressions for w , $g\left(\frac{T-T_0}{T_0}\right)$, R :

$$2\pi C^2 z^m z^{2l} z^n \int_0^\infty \text{function}\left(\frac{r}{R}\right) \times \text{another}\left(\frac{r}{R}\right) d\left(\frac{r}{R}\right) = F$$

This definite integral is just some number. No z -dependence (or even r dependence) in it.

And no z -dependence on r.h.s. so no z -dependence on l.h.s.

∴ $m + 2l + n = 0$

This is a constraint on the power laws.

Get more constraints on the power laws by working with the vertical comp of the eqⁿ of motion

$$w \frac{\partial w}{\partial z} \sim g \frac{(T-T_0)}{T_0} \sim \frac{\tau}{r} \frac{\partial}{\partial r} \frac{\partial w}{\partial r} \quad r = R\left(\frac{r}{R}\right)$$

accelⁿ buoyancy friction

$$\frac{1}{R^2} \frac{\partial}{\partial (r/R)} \frac{\partial}{\partial (r/R)} \left(\frac{r}{R}\right) \frac{\partial w}{\partial (r/R)}$$

just focus on the z -dependence, get

$$z^{2m-1} \sim z^n \sim z^{m-2l}$$

∴ $2m-1 = n = m-2l$

Together with other constraint for m, n, l , get 3 eqⁿs for 3 unknowns.

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$n = m - 2l$ plug into $m + 2l + n = 0$

$$\therefore m + 2l + m - 2l = 0$$

$$\therefore 2m = 0$$

$$\boxed{m = 0}$$

then use $2m - 1 = n$

$$\therefore \boxed{n = -1}$$

lastly $n = m - 2l$
 $\downarrow \quad \downarrow$
 $-1 \quad 0$

$$\therefore \boxed{l = 1/2}$$

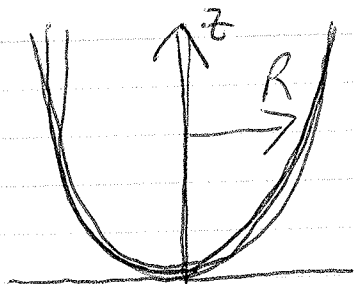
So:

$$\boxed{w = \text{function} \left(\frac{r}{R} \right)} \quad (\text{involving other governing parameters but NOT } z!)$$

$$\boxed{g \left(\frac{T - \bar{T}_0}{\bar{T}_0} \right) = \frac{1}{z} \text{function} \left(\frac{r}{R} \right)} \quad " "$$

$$\boxed{R = C \sqrt{z}} \quad " "$$

So plume looks like a parabola $(z \sim R^2)$



Now, to see how the other parameters enter the solution, use the P_i Theorem.